

# Airgas<sup>®</sup>

an Air Liquide company

## RSR- SSM IMPACTS COMPLIANCE AND OPTIMIZATION



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| Airgas, an Air Liquide company

| Refinery Sector Rule (RSR)

| SSM Impacts- Compliance and Optimization

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*'If you think Compliance is expensive, try non-compliance'*

Paul McNulty, former U.S. Deputy Attorney General

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# 1

## RSR for Flares - Overview

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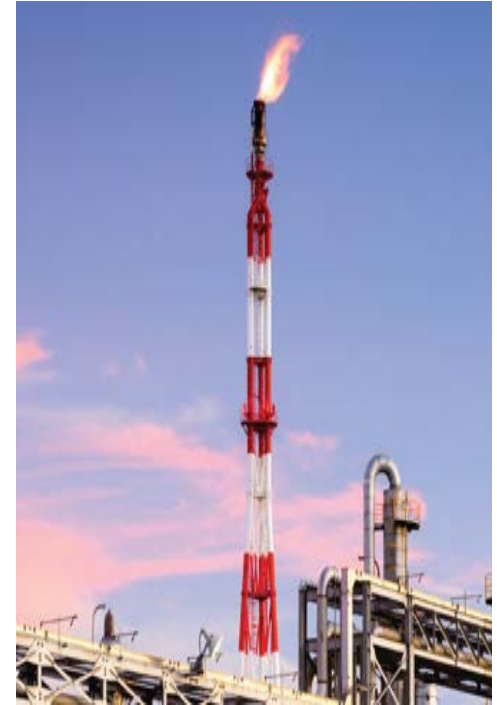
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# Refinery Sector Rule- Flares Overview

- **Most Comprehensive Rule Revision by EPA to Date**
  - Multiple sections applying to Fence line, Storage, Venting
  - Flare section focus:
    - Full combustion of Hazardous Air Pollutants (HAPs)
    - Increased Destruction Removal Efficiency (DRE)
- **Requirements to Monitor Net Heating Value (NHV)**
  - Installation of new monitoring systems
  - Must be  $\geq 270$  Btu adjusted NHV at flare tip in 15 minute blocks
  - Performance Spec and NHV calculation definitions
- **Requirements to Control NHV**
  - Startup, Shutdown & Malfunction (SSM) exemptions eliminated



■ 37. The appendix to subpart CC is amended by adding table 12 to read as follows:

**Appendix to Subpart CC of Part 63—  
Tables**

\* \* \* \* \*

“Table 12 Normalized  
Certificate of Analysis”

**TABLE 12—INDIVIDUAL COMPONENT PROPERTIES**

Component	Molecular formula	MW <sub>i</sub> (pounds per pound-mole)	CMN <sub>i</sub> (mole per mole)	NHV <sub>i</sub> (British thermal units per standard cubic foot)	LFL <sub>i</sub> (volume %)
Acetylene .....	C <sub>2</sub> H <sub>2</sub> .....	26.04	2	1,404	<b>GPA</b>
Benzene .....	C <sub>6</sub> H <sub>6</sub> .....	78.11	6	3,591	<b>NHV</b>
1,2-Butadiene .....	C <sub>4</sub> H <sub>6</sub> .....	54.09	4	2,794	
1,3-Butadiene .....	C <sub>4</sub> H <sub>6</sub> .....	54.09	4	2,690	
iso-Butane .....	C <sub>4</sub> H <sub>10</sub> .....	58.12	4	2,957	<b>3000</b>
n-Butane .....	C <sub>4</sub> H <sub>10</sub> .....	58.12	4	2,968	<b>3011</b>
cis-Butene .....	C <sub>4</sub> H <sub>8</sub> .....	56.11	4	2,830	
iso-Butene .....	C <sub>4</sub> H <sub>8</sub> .....	56.11	4	2,928	
trans-Butene .....	C <sub>4</sub> H <sub>8</sub> .....	56.11	4	2,826	
Carbon Dioxide .....	CO <sub>2</sub> .....	44.01	1	0	∞
Carbon Monoxide .....	CO .....	28.01	1	316	12.5
Cyclopropane .....	C <sub>3</sub> H <sub>6</sub> .....	42.08	3	2,185	2.4
Ethane .....	C <sub>2</sub> H <sub>6</sub> .....	30.07	2	1,595	<b>1619</b>
Ethylene .....	C <sub>2</sub> H <sub>4</sub> .....	28.05	2	1,477	<b>1499</b>
Hydrogen .....	H <sub>2</sub> .....	2.02	0	1,212 <sup>a</sup>	<b>274</b>
Hydrogen Sulfide .....	H <sub>2</sub> S .....	34.08	0	587	<b>4.0</b>
Methane .....	CH <sub>4</sub> .....	16.04	1	896	<b>909</b>
Methyl-Acetylene .....	C <sub>3</sub> H <sub>4</sub> .....	40.06	3	2,088	1.7
Nitrogen .....	N <sub>2</sub> .....	28.01	0	0	∞
Oxygen .....	O <sub>2</sub> .....	32.00	0	0	∞
Pentane+ (C5+) .....	C <sub>5</sub> H <sub>12</sub> .....	72.15	5	3,655	1.4
Propadiene .....	C <sub>3</sub> H <sub>4</sub> .....	40.06	3	2,066	<b>2.16</b>
Propane .....	C <sub>3</sub> H <sub>8</sub> .....	44.10	3	2,281	<b>2.1</b>
Propylene .....	C <sub>3</sub> H <sub>6</sub> .....	42.08	3	2,150	<b>2.4</b>
Water .....	H <sub>2</sub> O .....	18.02	0	0	∞

<sup>a</sup> The theoretical net heating value for hydrogen is 274 Btu/scf, but for the purposes of the flare requirement in this subpart, a net heating value of 1,212 Btu/scf shall be used.

# 2

## RSR for Flares - NHV Control SSM Impacts

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# NHV CONTROL

- Startup, Shutdown & Malfunction (SSM) exemption eliminated with RSR
- “The Rule now applies at all times”
- Potentially challenging to comply during major nitrogen purge events and steam outs
- Supplemental fuel gas likely needed to maintain 270 Btu during high N<sub>2</sub> flow purging and steam out events



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# PRINCIPLE OPTIONS-

Any individual or combination of

- Internal Supplemental Fuel Gas
- Reduce Purge Flow
- Thermal Oxidizers
- External Supplemental Fuel Gas



# NHV CONTROL-

## Internal Supplemental Fuel Gas

- Natural Gas, Light Ends (Fuel Gas), Hydrogen
- Challenges
  - Sufficiently available fuel gas
  - Proximity of fuel gas to flares
  - Capital cost for engineering, piping & infrastructure
  - Necessity to “dial back” purge flow to maintain compliance
- Potential Impacts
  - Ability to maintain compliance
  - Extended turnaround project cycle time
  - Increased turnaround costs - labor, rentals
  - Opportunity cost for major unit downtime



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# NHV CONTROL-

## Dial Back Flow Rate

- High Demand - Hydrocracker Purge
- 60%+/- Dial Back
- Extend project from 1 day to 3
- Opportunity Cost for Production Unit
- Extended Project/ Turnaround Time & Costs



## Thermal Oxidizer

- No to low emissions
- Large footprint
- Infrastructure
  - > Piping to divert flare stream
  - > High energy demand

# External Supplemental Fuel Gas (ESFG\*)

## PROJECT BASED

- Single point connection
- Plug and Play
- No utility set up for power, water, steam or gas
- Low capital
- Process downtime and turnaround project time
- Lower gas volume requirements vs. optional fuels

## COMPLIANCE

- Ability to stay above required NHV levels
- EPA compliant flow monitoring and low sulfurs fuel



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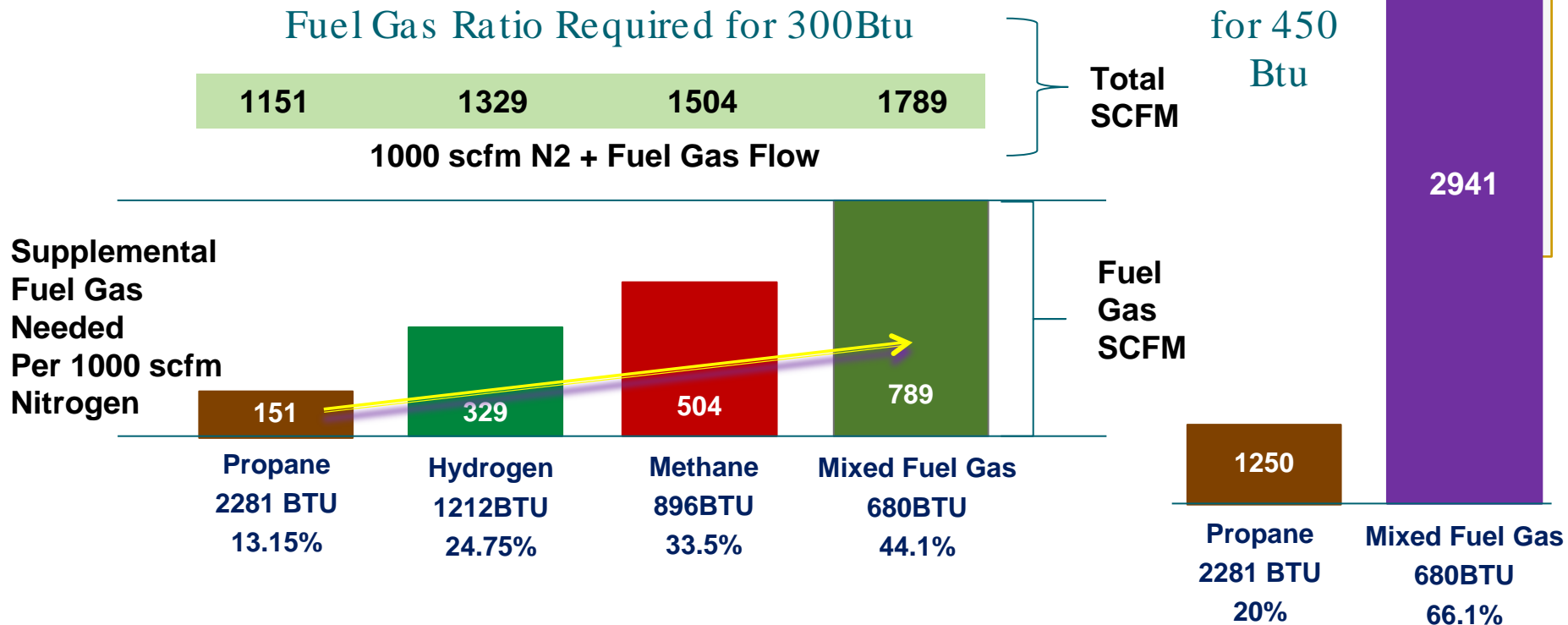
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# Alternative Fuel Gas Ratio Requirements



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# External Supplemental Fuel Gas (ESFG)



Liquid Fuel Gas Supply



Trailer Mounted Vaporization



Control Manifold with EPA  
Compliant Flow Monitoring



Thank you

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